

# TNSolver Command Summary

## Begin Solution Parameters

```

title           = (S ...)
type           = {<steady>|transient}
units          = {<SI>|US}
T units        = {<C>|K|F|R}
nonlinear convergence = {<1.0E-9>|(R)}
maximum nonlinear iterations = {<100>|(I)}
begin time     = {<0.0>|(R)}
end time       = (R)
time step      = (R)
number of time steps = (I)
print interval = {<1>|(I)}
Stefan-Boltzmann = {<5.6704E-8 W/m^2-K^4>|1.714e-9 Btu/hr-ft^2-R^4}
gravity        = {<9.80665 m/s^2>|32.174 ft/s^2}
graphviz output = {<no>|yes}
plot functions = {<no>|yes}

```

## End Solution Parameters

## Begin Nodes

```

! label material volume
  (S)      (S)      (R)

! label density*specific heat volume
  (S)      (R)      (R)

```

## End Nodes

## Begin Conductors

```

! label type nd_i nd_j parameters
  (S) conduction (S) (S) (R) (R) (R) ! k, L, A
  (S) conduction (S) (S) (S) (R) (R) ! material, L, A
  (S) cylindrical (S) (S) (R) (R) (R) (R) ! k, ri, ro, L
  (S) cylindrical (S) (S) (S) (R) (R) (R) ! material, ri, ro, L
  (S) spherical (S) (S) (R) (R) (R) ! k, ri, ro
  (S) spherical (S) (S) (S) (R) (R) ! material, ri, ro

  (S) convection (S) (S) (R) (R) ! h, A
  (S) IFCduct (S) (S) (S) (R) (R) (R) ! material, velocity, Dh, A
  (S) EFCcyl (S) (S) (S) (R) (R) (R) ! material, velocity, D, A
  (S) EFCdiamond (S) (S) (S) (R) (R) (R) ! material, velocity, D, A
  (S) EFCimpjet (S) (S) (S) (R) (R) (R) (R) ! material, velocity,
    ! D, H, r
  (S) EFCplate (S) (S) (S) (R) (R) (R) (R) ! material, velocity,
    ! Xbegin, Xend, A
  (S) EFCsphere (S) (S) (S) (R) (R) ! material, velocity, D

```

```

(S) INCvenc (S) (S) (S) (R) (R) (R) ! material, W, H, A
(S) ENChcyl (S) (S) (S) (R) (R) ! material, D, A
(S) ENChplatedown (S) (S) (S) (R) (R) ! material, L=A/P, A
(S) ENChplateup (S) (S) (S) (R) (R) ! material, L=A/P, A
(S) ENCIplatedown (S) (S) (S) (R) (R) (R) (R) ! material, H, L=A/P,
    ! angle, A
(S) ENCIplateup (S) (S) (S) (R) (R) (R) (R) ! material, H, L=A/P,
    ! angle, A
(S) ENCsphere (S) (S) (S) (R) ! material, D
(S) ENCVplate (S) (S) (S) (R) (R) ! material, L, A
(S) FCuser (S) (S) (S) (S) (R ...) (R) ! function, material,
    ! parameters, A
(S) NCuser (S) (S) (S) (S) (R ...) (R) ! function, material,
    ! parameters, A

(S) surfrad (S) (S) (R) (R) ! emissivity, A
(S) radiation (S) (S) (R) (R) ! script-F, A

(S) advection (S) (S) (S) (R) (R) ! material, velocity, A
(S) outflow (S) (S) (S) (R) (R) ! material, velocity, A

```

## End Conductors

## Begin Boundary Conditions

```

! type parameter node(s)
fixed_T (R) (S ...) ! T
heat_flux (R) (R) (S ...) ! q, A

```

## End Boundary Conditions

## Begin Sources

```

! type parameter(s) node(s)
qdot (R) (S ...) ! q-dot, uses node volume: Q = qV
Qsrc (R) (S ...) ! Q
tstatQ (R) (S) (R) (R) (S ...) ! Q, thermostat node, Ton, Toff

```

## End Sources

## Begin Initial Conditions

```

! Initial T node(s)
  (R) all ! apply to all nodes in the model
  (R) (S ...)
read_restart = (S) ! read T from restart file

```

## End Initial Conditions

# TNSolver Command Summary

```

Begin Radiation Enclosure

! label emiss area view factors
  (S) (R) (R) (R ...)

End Radiation Enclosure

Begin Functions

  Begin Constant (S) ! function name
    (R)
  End Constant (S)

  Begin Time {Table|Spline} (S) ! function name
! time value
  (R) (R)
  ...
  (R) (R)
  End Time {Table|Spline} (S)

  Begin Polynomial (S) ! function name
    (R ...) ! a0 a1 a2 ...
    range = (R) (R) ! range begin and end
  End Polynomial (S)

  Begin Composite (S) ! function name
    (S ...) ! list of function names
  End Composite (S)

End Functions

Begin Material (S) ! material name

  State = (S) ! {gas|liquid|solid}, required for all materials

  Density = {(R)|ideal gas} ! ideal gas:  $\rho = P/RT$ 
  Density {Table|Spline}
! T density
  (R) (R)
  ...
  (R) (R)
  End Density {Table|Spline}
  Density Polynomial
  (R ...) ! a0 a1 a2 ...
  range = (R) (R) ! range begin and end
  End Density Polynomial

  Conductivity = (R)
  Conductivity {Table|Spline}

```

```

! T k
  (R) (R)
  ...
  (R) (R)
  End Conductivity {Table|Spline}
  Conductivity Polynomial
  (R ...) ! a0 a1 a2 ...
  range = (R) (R) ! range begin and end
  End Conductivity Polynomial

  {Specific Heat|c.v} = (R) ! constant volume specific heat
  {Specific Heat|c.v} {Table|Spline}
! T c.v
  (R) (R)
  ...
  (R) (R)
  End {Specific Heat|c.v} {Table|Spline}
  {Specific Heat|c.v} Polynomial
  (R ...) ! a0 a1 a2 ...
  range = (R) (R) ! range begin and end
  End {Specific heat|c.v} Polynomial

  c.p = (R) ! constant pressure specific heat
  c.p {Table|Spline}
! T c.p
  (R) (R)
  ...
  (R) (R)
  End c.p {Table|Spline}
  c.p Polynomial
  (R ...) ! a0 a1 a2 ...
  range = (R) (R) ! range begin and end
  End c.p Polynomial

  Viscosity = (R) ! dynamic viscosity:  $\mu$ 
  Viscosity {Table|Spline}
! T viscosity,  $\mu$ 
  (R) (R)
  ...
  (R) (R)
  End Viscosity {Table|Spline}
  Viscosity Polynomial
  (R ...) ! a0 a1 a2 ...
  range = (R) (R) ! range begin and end
  End Viscosity Polynomial

  Beta = {(R)|ideal gas} ! thermal expansion coefficient,
  ! ideal gas:  $\beta = 1/T$ 
  Beta {Table|Spline}

```

# TNSolver Command Summary

```

!   T   beta,  $\beta$ 
    (R) (R)
    ...
    (R) (R)
End Beta {Table|Spline}
Beta Polynomial
    (R ...) ! a0 a1 a2 ...
    range = (R) (R) ! range begin and end
End Beta Polynomial

Pr = (R) ! Prandtl number,  $Pr = c_p\mu/k$ 
Pr {Table|Spline}
!   T   Pr,  $Pr = c_p\mu/k$ 
    (R) (R)
    ...
    (R) (R)
End Pr {Table|Spline}
Pr Polynomial
    (R ...) ! a0 a1 a2 ...
    range = (R) (R) ! range begin and end
End Pr Polynomial

gas constant = (R) ! gas constant for use with ideal gas:  $R = \hat{R}/M$ 

reference = (S ...)

End Material (S)

```

## Units

|            | SI               | US                                 |
|------------|------------------|------------------------------------|
| $t$        | $s$              | $hr$                               |
| $L, D$     | $m$              | $ft$                               |
| $A$        | $m^2$            | $ft^2$                             |
| $V$        | $m^3$            | $ft^3$                             |
| $\rho$     | $kg/m^3$         | $lb_m/ft^3$                        |
| $c_v, c_p$ | $J/kg \cdot K$   | $Btu/lb_m \cdot ^\circ R$          |
| $k$        | $W/m \cdot K$    | $Btu/hr \cdot ft \cdot ^\circ R$   |
| $\mu$      | $kg/m \cdot s$   | $lb_m/ft \cdot hr$                 |
| $h$        | $W/m^2 \cdot K$  | $Btu/hr \cdot ft^2 \cdot ^\circ R$ |
| $T$        | $C = K - 273.15$ | $^\circ F = ^\circ R - 459.67$     |
| $Q$        | $W$              | $Btu/hr$                           |
| $q$        | $W/m^2$          | $Btu/hr \cdot ft^2$                |
| $\dot{q}$  | $W/m^3$          | $Btu/hr \cdot ft^3$                |
| $u, v, w$  | $m/s$            | $ft/hr$                            |

## Dimensionless Numbers

$$Pr = \frac{\text{viscous diffusion rate}}{\text{thermal diffusion rate}} = \frac{c_p\mu}{k} = \frac{\nu}{\alpha} = \frac{\mu/\rho}{k/(\rho c_p)}$$

$$Nu_L = \frac{\text{convective heat transfer}}{\text{conductive heat transfer}} = \frac{hL}{k}$$

$$Re_L = \frac{\text{inertial forces}}{\text{viscous forces}} = \frac{\rho uL}{\mu} = \frac{uL}{\nu}$$

$$D_h = \frac{4 \times \text{cross-sectional area}}{\text{wetted perimeter}} = \frac{4A_c}{P}$$

$$Gr_L = \frac{g\rho^2\beta L^3\Delta T}{\mu^2} = \frac{g\beta L^3\Delta T}{\nu^2}$$

$$Ra_L = Gr_L Pr = \frac{c_p\rho^2 g\beta L^3\Delta T}{\mu k} = \frac{g\beta L^3\Delta T}{\nu\alpha}$$

$$Bi = \frac{hL_c}{k} < 0.1 \quad L_c = \frac{V}{A} \quad Fo = \frac{\alpha t}{L_c^2} = \frac{kt}{\rho c L_c^2}$$

## Command Description Character Symbols

|         |   |
|---------|---|
| { }     | list of valid parameters                    |
| < >     | default parameter in the list of parameters |
|         | separator for the list of valid parameters  |
| (I)     | single integer number                       |
| (I ...) | list of integer numbers                     |
| (R)     | single real number                          |
| (R ...) | list of real numbers                        |
| (S)     | single character string                     |
| (S ...) | list of character strings                   |

## Conversion Factors

|      |   |                                |
|------|---|--------------------------------|
| 1 s  | = | 0.0002777778 hr                |
| 1 m  | = | 3.28084 ft                     |
| 1 kg | = | 2.204623 lb <sub>m</sub>       |
| 1 K  | = | 1.8 °R                         |
| C    | = | $\frac{5}{9} (^{\circ}F - 32)$ |
| 1 J  | = | 0.00094781712 BTU              |
| 1 W  | = | 3.412142 BTU/hr                |

# TNSolver Command Summary

| Quantity                        | SI   | Multiply by             | US  |
|---------------------------------|--|-------------------------|---|
| time, $t$                       | $s$  | $\times 0.000277778 =$  | $hr$  |
| length, $L$                     | $m$  | $\times 3.2808399 =$    | $ft$  |
| area, $A$                       | $m^2$  | $\times 10.76391 =$     | $ft^2$                                      |
| volume, $V$                     | $m^3$  | $\times 35.314667 =$    | $ft^3$                                      |
| temperature, $T$                | $K$  | $\times 1.8 =$          | $^{\circ}R$                                 |
| density, $\rho$                 | $\frac{kg}{m^3}$   | $\times 0.062427961 =$  | $\frac{lb_m}{ft^3}$                         |
| thermal conductivity, $k$       | $\frac{W}{m \cdot K}$                                      | $\times 0.57778932 =$   | $\frac{hr \cdot ft \cdot ^{\circ}R}{Btu}$   |
| specific heat, $c_v, c_p$       | $\frac{J}{kg \cdot K}$                                     | $\times 0.0002388459 =$ | $\frac{lb_m \cdot ^{\circ}R}{Btu}$          |
| viscosity, $\mu$                | $Pa \cdot s$ or $\frac{N \cdot s}{m^2}$                    | $\times 2419.0883 =$    | $\frac{lb_m}{ft \cdot hr}$                  |
| thermal expansion, $\beta$      | $\frac{1}{K}$  | $\times 0.555556 =$     | $\frac{1}{^{\circ}R}$                       |
| convection coefficient, $h$     | $\frac{W}{m^2 \cdot K}$ or $\frac{J}{s \cdot m^2 \cdot K}$ | $\times 0.17611018 =$   | $\frac{Btu}{hr \cdot ft^2 \cdot ^{\circ}R}$ |
| heat flux, $q$                  | $\frac{W}{m^2}$ or $\frac{J}{s \cdot m^2}$                 | $\times 0.31699833 =$   | $\frac{Btu}{hr \cdot ft^2}$                 |
| rate of heat transfer, $Q = qA$ | watt ( $W$ ) or $\frac{J}{s}$                              | $\times 3.4121416 =$    | $\frac{Btu}{hr}$                            |

## Practical Values

| Temperature |       | Velocity |         | Pressure |           |
|-------------|-------|----------|---------|----------|-----------|
| F           | C     | mph      | m/s     | psi      | Pa        |
| 0.0         | -17.8 | 1.0      | 0.44704 | 1.0      | 6,894.8   |
| 32.0        | 0.0   | 5.0      | 2.2352  | 5.0      | 34,473.8  |
| 70.0        | 21.1  | 10.0     | 4.4704  | 14.696   | 101,325.0 |
| 100.0       | 37.8  | 20.0     | 8.9408  | 50.0     | 344,737.9 |
| 212.0       | 100.0 | 50.0     | 22.352  | 100.0    | 689,475.7 |
|             |       | 100.0    | 44.704  |          |           |

## Parameters Replaceable by Functions

| Nodes               |                  |
|---------------------|------------------|
|                     | $\rho C$ and $V$ |
| Boundary Conditions |                  |
| fixed_T             | $T_b$            |
| heat_flux           | $q$ and $A$      |
| Sources             |                  |
| qdot                | $\dot{q}$        |
| Qsrc                | $Q$              |

## Material Property Library

| material | Notes                                |
|----------|--------------------------------------|
| air      | At atmospheric pressure, 101.325 kPa |
| water    |                                      |
| steel    | AISI 1010                            |
| fir      | Perpendicular to the grain           |